

Total No. of Questions : 10]

SEAT No. :

**P2902**

**[4958]-1095**

[Total No. of Pages : 4

**T.E. (Chemical Engg.)  
MASS TRANSFER - I  
(2012 Course) (Semester - I)**

*Time : 2½ Hours]*

*[Max. Marks : 70*

*Instructions to the candidates:*

- 1) *Neat diagrams must be drawn wherever necessary.*
- 2) *Figures to the right indicate full marks.*
- 3) *Use of logarithmic tables slide rule, Mollier charts, electronic pocket Calculator and steam tables is allowed.*
- 4) *Assume suitable data, if necessary.*

- Q1) a)** A gas mixture containing one fifth hydrogen and four fifth methane by volume is prepared, through which oxygen is allowed to diffuse. The total pressure is  $1 \times 10^5$  N/m<sup>2</sup> and temperature is 2°C. Estimate the rate of diffusion of oxygen through a film of gas mixture, 3 mm thick when the concentration change across the film is 12 to 7% by volume. The diffusivity are,  $D_{O_2-H_2} = 7.1 \times 10^{-5}$  m<sup>2</sup>/sec.  $D_{O_2-CH_4} = 1.88 \times 10^{-5}$  m<sup>2</sup>/sec. **[5]**
- b) State Fick's First law of diffusion. Derive an expression for steady state equimolar counter current Diffusion. **[5]**

OR

- Q2) a)** Ammonia gas is diffusing through a layer of stagnant air, 2.5mm thick at constant rate. Conditions are fixed so that gas contains 50% ammonia by volume a one boundary of stagnant layer. Ammonia is quickly absorbed on other side and its concentration is negligible at that plane. The temperature is 20°C and pressure is atmospheric. The diffusivity for ammonia-air system is 0.18 cm<sup>2</sup>/sec. Calculate the rate of diffusion of ammonia through air in gm. mole/hr.cm<sup>2</sup> **[5]**
- b) Write short note on Chilton-Colburn Analogy and Reynolds Analogy. **[5]**

**P.T.O.**

- Q3) a)** Define absorption factor and stripping factor. [2]
- b) Ammonia is absorbed by water in wetted wall column using operating temperature of 20°C and 1 atm pressure. The overall coefficient is  $2.72 \times 10^{-4}$  kmol/m<sup>2</sup> atm. At one point in the column the gas contained 10mol% ammonia and the liquid phase concentration was  $6.42 \times 10^{-2}$  kmol ammonia per m<sup>3</sup> of solution. Temperature is 20°C and 1 atm pressure. 85% of the resistance to mass transfer lies in a gas phase. If Henry's law constant is  $9.35 \times 10^{-3}$  atm m<sup>3</sup>/kmol, calculate the individual film coefficient and the interfacial composition. [8]

OR

- Q4)** A mixture of Acetone vapor and air contain 5% by volume of acetone is to be freed from acetone content by scrubbing it with water in a absorption column. The flow rate of gas mixture is 700 m<sup>3</sup>/hr of acetone free air measured at NTP and that of water is 1500 kg/ hr. the absorber operates at an average temperature of 20°C and a pressure of 101 KPa. The scrubber absorbs 98% acetone. The equilibrium relation for the acetone-water system is  $Y^* = 1.68 X$ , where  $Y =$  Kmol of acetone/kmol of dry air,  $X =$  Kmol of acetone/kmol of water, calculate
- a) mean driving force for absorption,
- b) mass transfer area if overall mass transfer coefficient is  $K_G = 0.4$  kmol of acetone/m<sup>2</sup>. hr [10]
- Q5) a)** 30000 m<sup>3</sup> of gas at 298°K and 101.3 kN/m<sup>2</sup> saturated with water vapor is compressed to 340 kN/m<sup>2</sup>, cooled to 289°K and condensed water is drained off. Subsequently the pressure is reduced to 170 kN/m<sup>2</sup> and the gas is distributed at this pressure and temp. What is % humidity. The vapor pressure of water at 289°K is 1.8 kN/m<sup>2</sup>. [8]
- b) Define:
- i) adiabatic saturation temperature,
- ii) enthalpy,
- iii) humid heat,
- iv) humid volume. [4]
- c) What are different types of cooling tower? Discuss spray chamber in brief. [4]

OR

**Q6) a)** Acetone is evaporated into a stream of nitrogen gas and this mixture of acetone vapor and nitrogen flows through a duct of cross section  $0.08\text{m}^2$ . The pressure and dry bulb temperature at one point in the duct are  $800\text{mm Hg}$  and  $45^\circ\text{C}$ . At this point the average velocity is  $4\text{ m/s}$ , the wet bulb temperature is  $28^\circ\text{C}$ . Calculate the mass flow rate of acetone vapor carried by duct. The data given: latent heat of vaporization for acetone =  $403000\text{ J/kg}$ ,  $h_g/K_y = 1700\text{ J/kg}^\circ\text{K}$ , vapor pressure of acetone =  $50\text{mm Hg}$ . [8]

b) Define wet bulb temperature and psychrometric ratio. Derive an expression relating wet bulb temp with absolute humidity and psychrometric ratio. [8]

**Q7) a)** Define

i) Murphree tray efficiency,

ii) Overall tray efficiency,

iii) Coning,

iv) Weeping. [8]

b) What are different types of trays used in column? Explain working of any one. [4]

c) Explain the end effects of axial mixing. [4]

OR

**Q8) a)** With neat sketch explain

i) Wetted Wall Column,

ii) Mechanically Agitated Vessels [8]

b) Compare packed and plate columns. [6]

c) What is pressure drop in column? Brief about positive and negative effects of pressure drop. [2]

- Q9) a)** Under constant drying conditions, a wet solid is dried from 30% to 4%. The time taken is 4 hours. All are on dry basis. The equilibrium moisture content is 2%. Critical moisture content is 10%. How long it takes to dry to 7%? Assume falling rate period is linear. **[10]**
- b) Give classification of drying equipments and working of fluidized bed dryer. **[6]**
- c) What are the factors affecting the rate of drying? **[2]**

OR

- Q10)a)** Data on drying rate curve of a particular solid is given below. The weight of the dry material in the solid is  $48 \text{ kg/m}^2$ . Calculate the time required to dry the material from 25% to 8% moisture (dry basis) **[10]**

kg/kg dry solid (X)	0.30	0.20	0.18	0.15	0.14	0.11	0.07	0.05
kg/hr.m <sup>2</sup> (N)	1.22	1.22	1.14	0.90	0.80	0.56	0.22	0.05

- b) Explain rate of drying curve with neat sketch. **[6]**
- c) What are the uses of drying operation? **[2]**

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